

Worldwide Pollution Control Association

ESKOM Scrubber Seminar
April 12th – 13th, 2007



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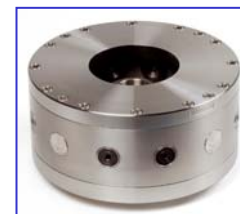
WPCA Seminar for ESKOM

**Semi-dry scrubber technologies:
Spray Drying Absorption**

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&
Mogens Rübner-Petersen

Niro A/S, Copenhagen, Denmark

April 13, 2007





Spray Drying Absorption:

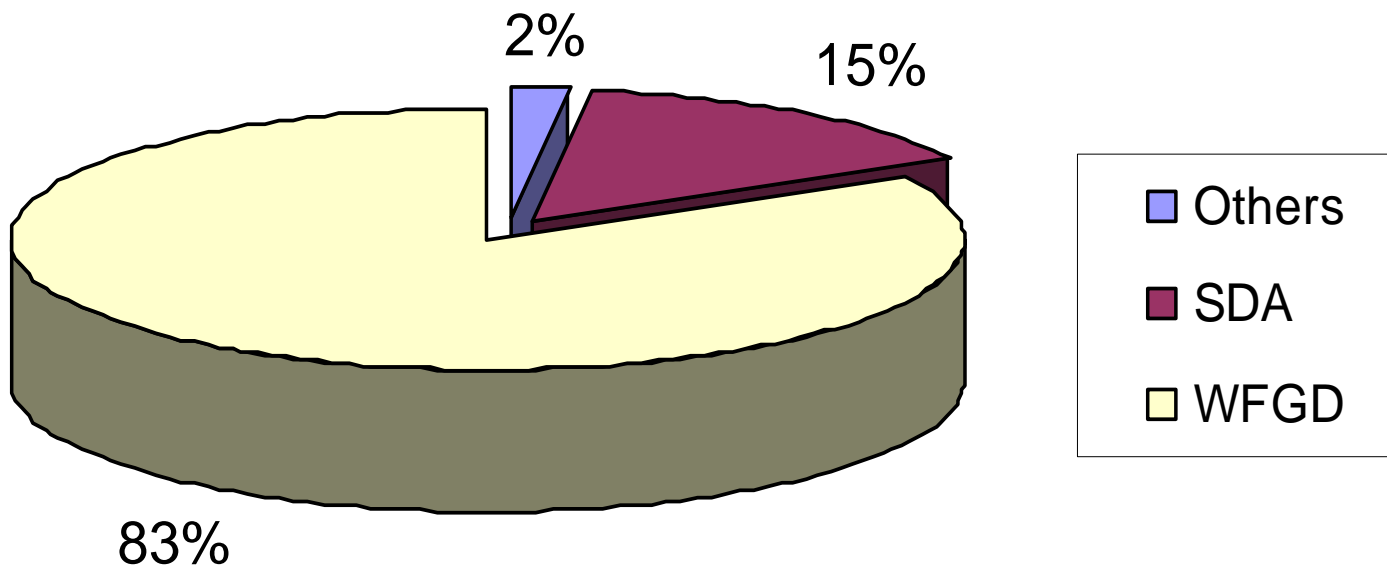
- Introduction
- Process Capabilities
- SDA Process
- Process Layout
- Main Components
- SDA Applications





Introduction

World Market Share of FGD Technologies Power applications



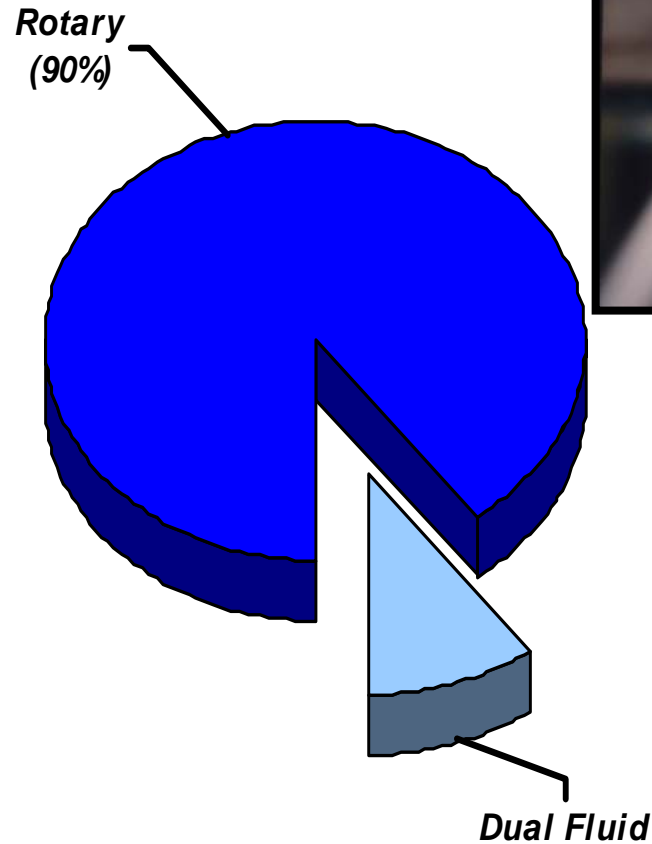


Rotary Atomizer

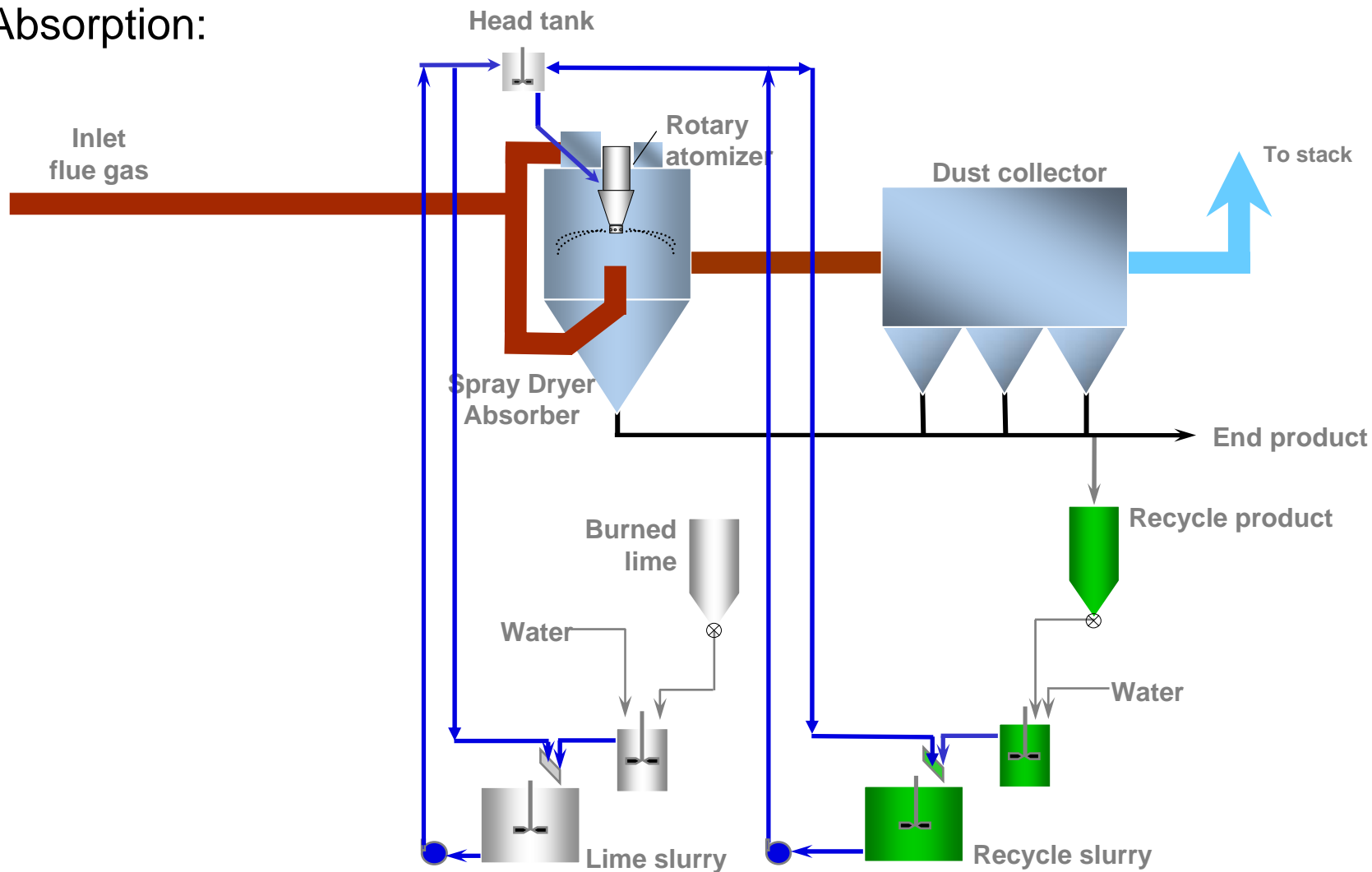


Dual Fluid

Installations share
by atomizer type



Spray Drying Absorption:





Process Capabilities

SDA – Especially applicable for:

- Medium to large size boilers, 100 MW and up
- Low to Medium Sulphur content in coal, 0 – 3 %
- Medium to high SO₂ removal rate requirement, up to 98%
- Extreme removal requirements of HCl, HF, SO₃ , > 99 %
- Plants with process water shortage and / or low quality process water supply (waste water, sea water brackish water)

SDA Main Design Parameters:

Plants	Power Plants, Waste Incinerators, Metal Processing Plants
Fuel	Coal, Lignite, Oil, Municipal Waste. Also applicable for industrial off-gases.
S-content in fuel	Optimized for coal S contents up to 3 %
SO ₂ – content in flue gas	Optimized for 0 – 7.000 mg/Nm ³ (0 – 2.500 ppm)
Air toxics	The SDA can be designed for any load of SO ₃ , HCl, HF, Hg etc.
Dust Load	< 15 g/Nm ³ : No precollection > 15 g/Nm ³ : Precollection considered
Flue Gas Inlet Temperature	Utility boilers: < 200 °C Industrial plants: < 450 °C
Process Water	The SDA makes use of any quality of process water, incl. sea water, brackish water, river water, waste water etc.

Actual experience ranges at power plants

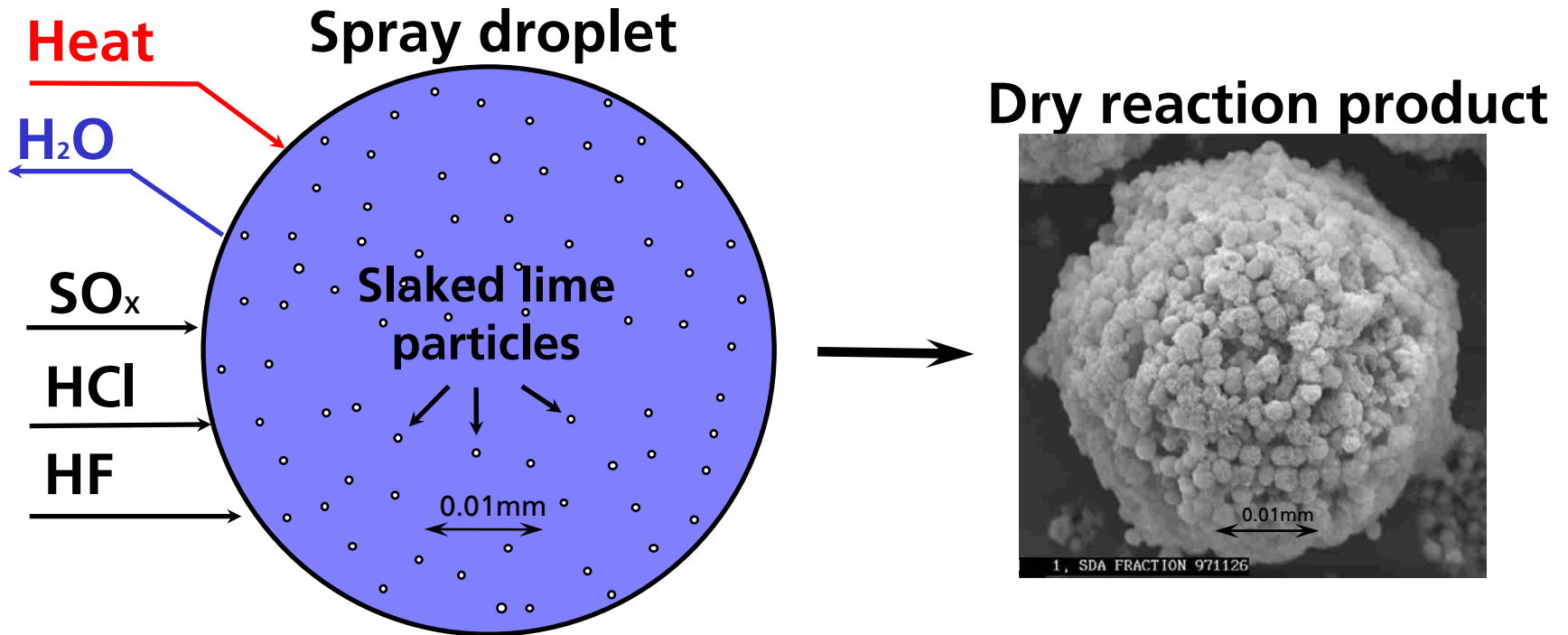
Parameter	Unit	Range
Total Flue Gas Flow rate	Nm ³ /h	18.000 – 4.300.000
Max. Flow rate per absorber module	Nm ³ /h	1.100.000 *)
Flue Gas Inlet temperature	°C	92 - 182
Coal Sulphur content	%wt.	0,2 – 3,5

*) SDA plant designed for 1.250.000 Nm³/h is under construction at Comanche Unit 3, USA. Latest Niro design accepts 1.600.000 Nm³/h per absorber.

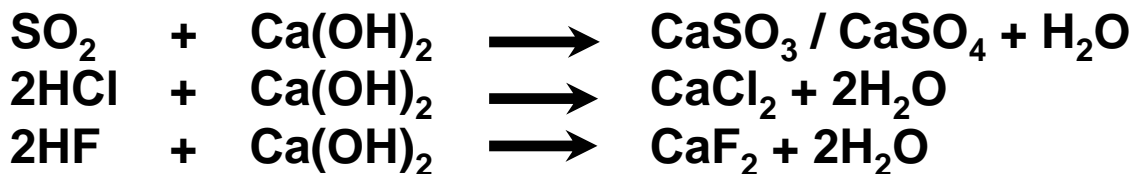
Parameter	Inlet Conc. [mg/Nm ³]	Removal rate [%]	Emission [mg/Nm ³]
SO ₂	800-7.000	> 99	< 10
SO ₃	< 10	> 99	< 1
HCl	< 125	> 99	< 1
HF	< 60	> 99	< 0,5
Hg	2 – 10 x 10 ⁻³	> 99	< 0,03 x 10 ⁻³



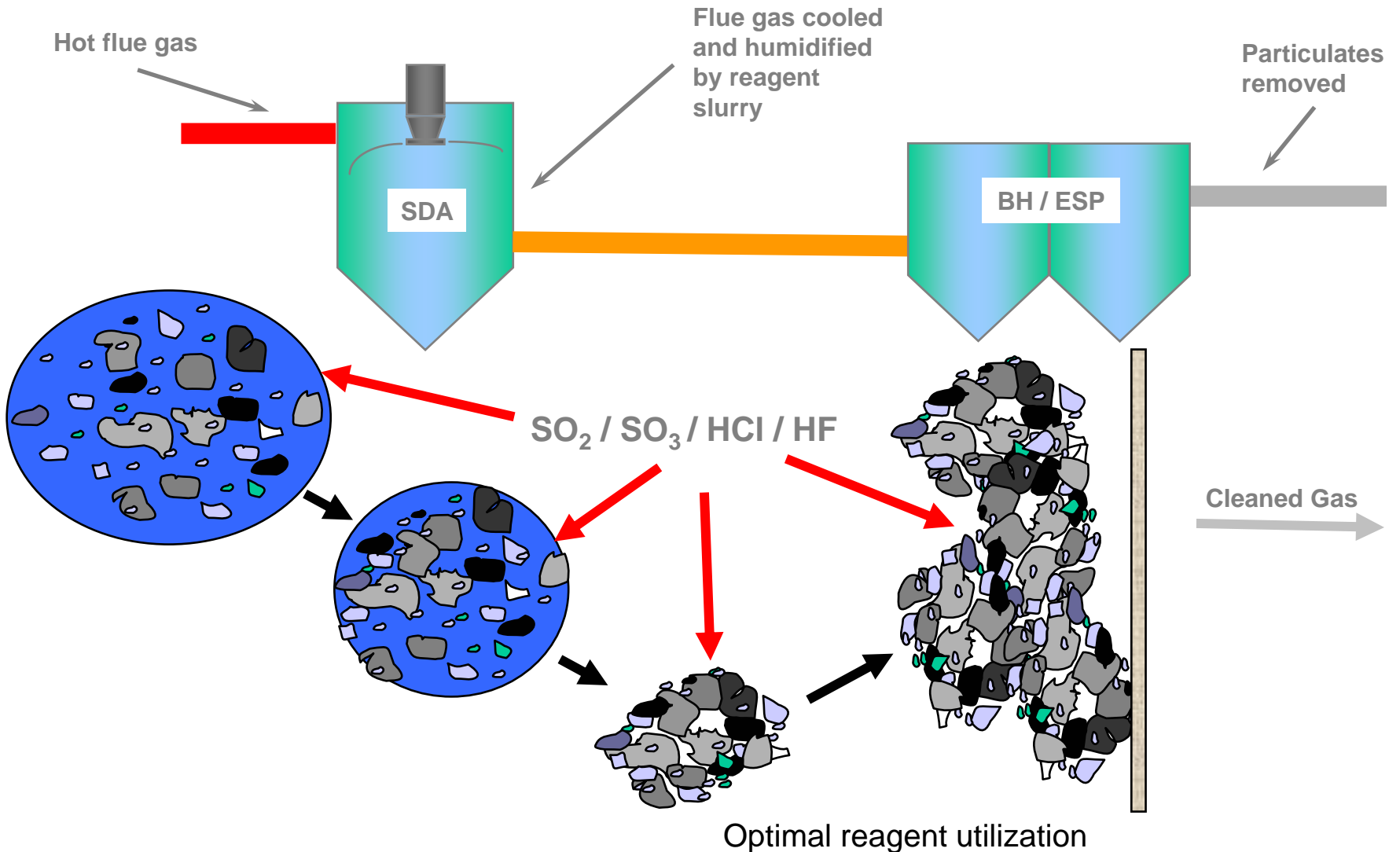
SPRAY DRYING ABSORPTION PROCESS



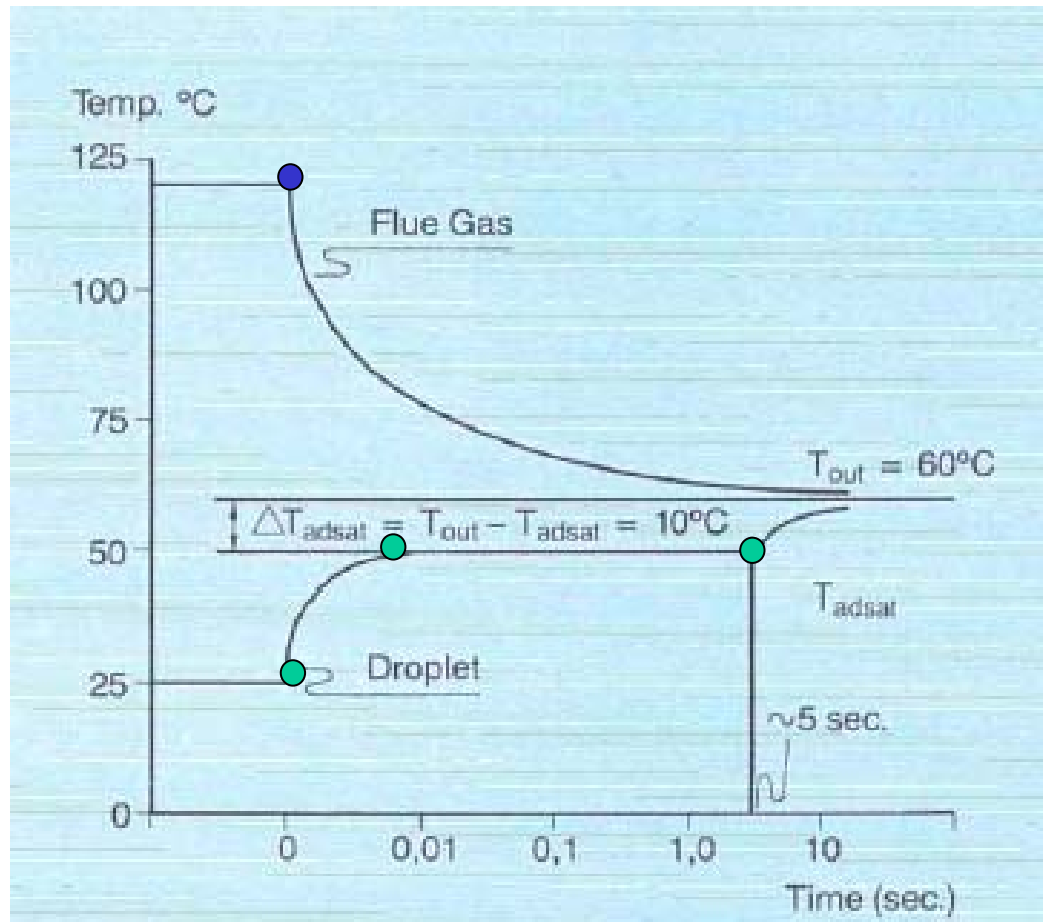
Main Reactions:



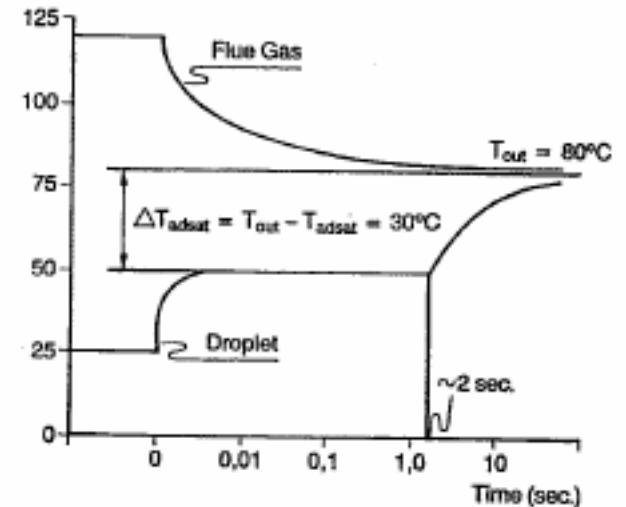
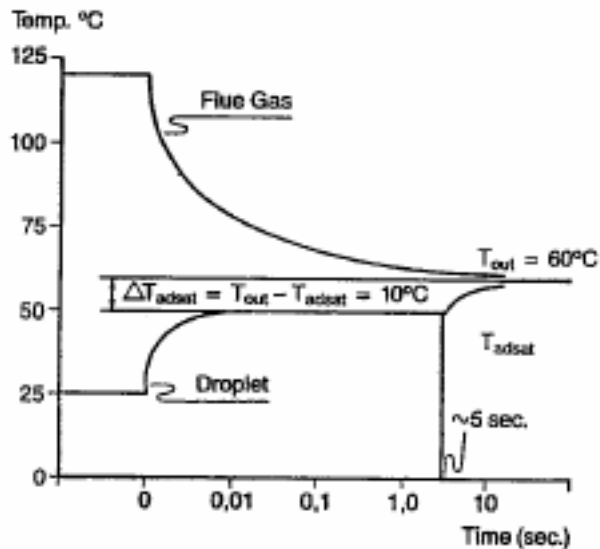
SDA - Two Stage Absorption Process



Influence of SDA outlet temperature

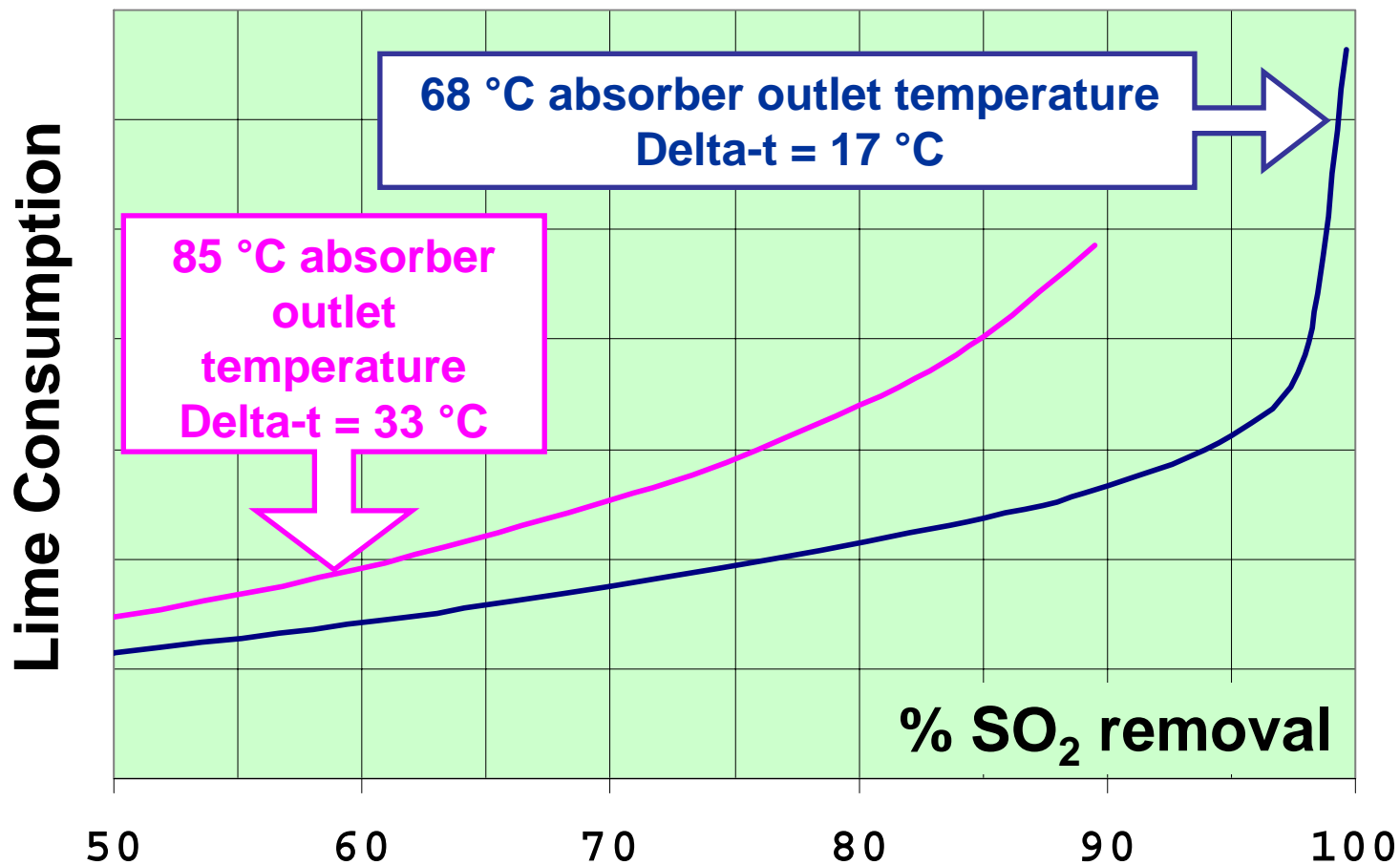


Approach to Adiabatic Saturation



Influence on drying time of difference between Spray Drying Absorber outlet temperature and adiabatic saturation temperature (ΔT_{adsat}).

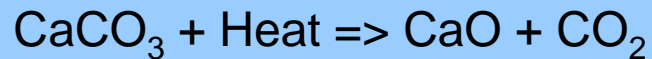
Lime Consumption vs SO₂ Removal Efficiency



SDA Absorbents:

- Burned lime, CaO (aka quicklime)
- Hydrated lime Ca(OH)₂
- Carbide lime

- Calcination of limestone:



- Hydration of burned lime:



Lime Quality:

➤ Purity

Preferably > 80 % available CaO. Lime with low purity is acceptable for the SDA, but the consumption will increase.

➤ Reactivity

Preferably T60 < 3 minutes, according to DIN 1080. If reactivity of the lime is lower, the consumption of lime may increase for maintained deSO_x-performance.

➤ Particle Size Distribution

The slaking process depends on the PSD of the available lime. Fine lime (< 1-3 mm) may be slaked in an ordinary tank or detention slaker. Paste slakers are widely used for optimum control of the slaking process. If lime particles are coarser, milling is an option.

SDA Process Water Quality:

Primary uses: Lime slaking and cooling of the flue gas.

Introduced to: The atomizer, via the lime slaking system (~20 %) and the recycle slurry system (~80 %).

Main parameters: Chloride content, due to corrosivity and its process enhancing characteristics.

Other parameters: For the lime slaking water, the sulphate content and the hardness are of importance to the detailed process design, due to sulphate's influence on the slaking process and the scaling potential of hard water.

Generally, river- or lake water is appropriate as lime slaking water source, and sea water is advantageous as water for the recycle slurry system.

Typical SDA Product composition

SDA Product Composition	Some precollection of fly ash	No precollection of fly ash
CaSO_3	35 - 60	15-30
CaSO_4	6 - 15	3-8
CaCl_2	0.1 – 2	0.1-1
CaCO_3	1 – 5	0.5-3
Ca(OH)_2	2 – 10	2-10
Free water	1 – 3	1-3
Bound water (crystal water)	4 – 10	2-6
Fly ash	1 – 30	50-80



Use of SDA product:

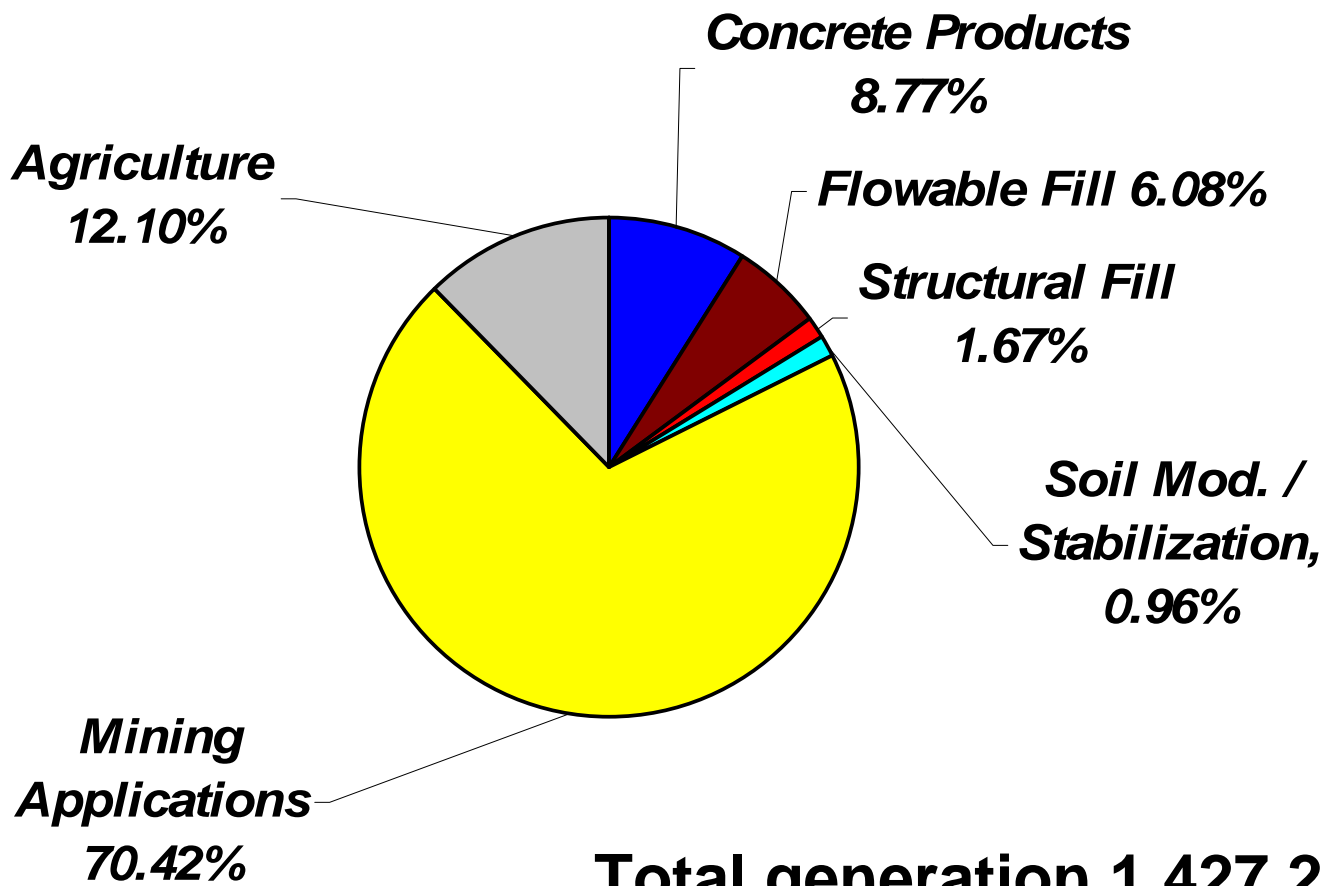
1 Disposal/use as filler:

- Land reclamation
- Mining back-fill

2 Utilization of SDA product:

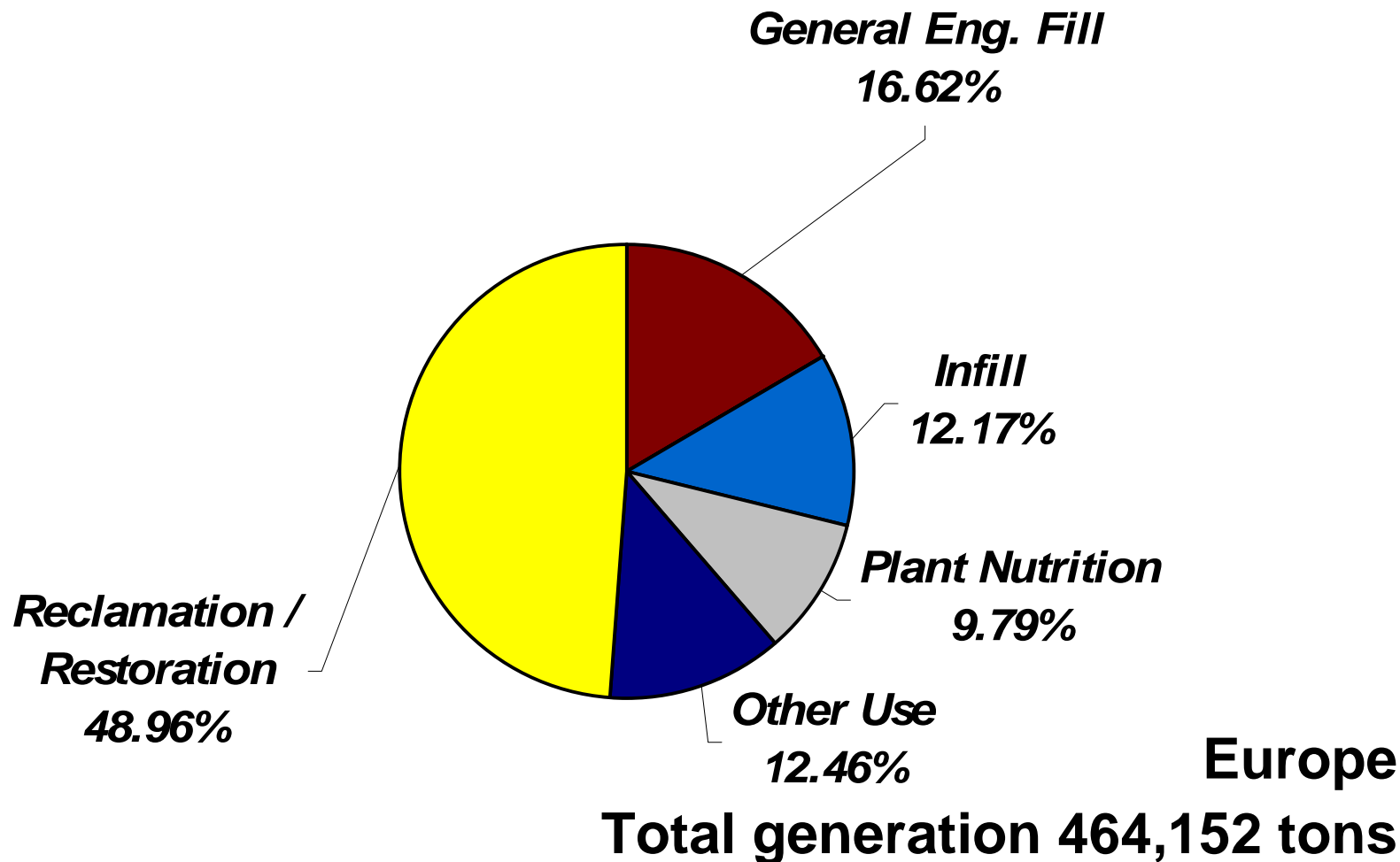
- Fertilizer
- Oxidation to gypsum.
- Building materials.
- Road construction base
- Noise and dust barriers
- Cat litter.
- Sulphuric acid.

SDA By-Product Solids Use (2005)

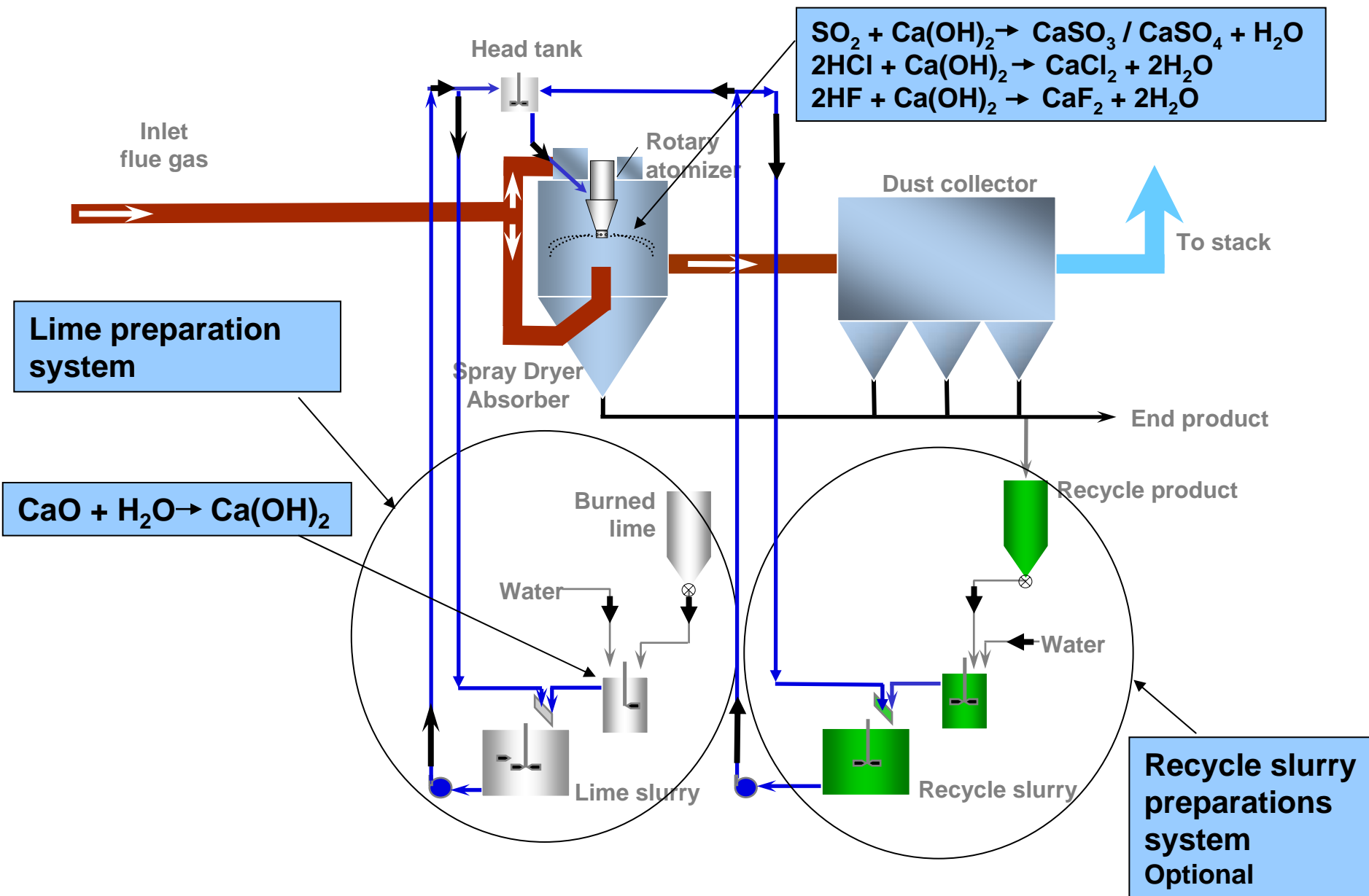


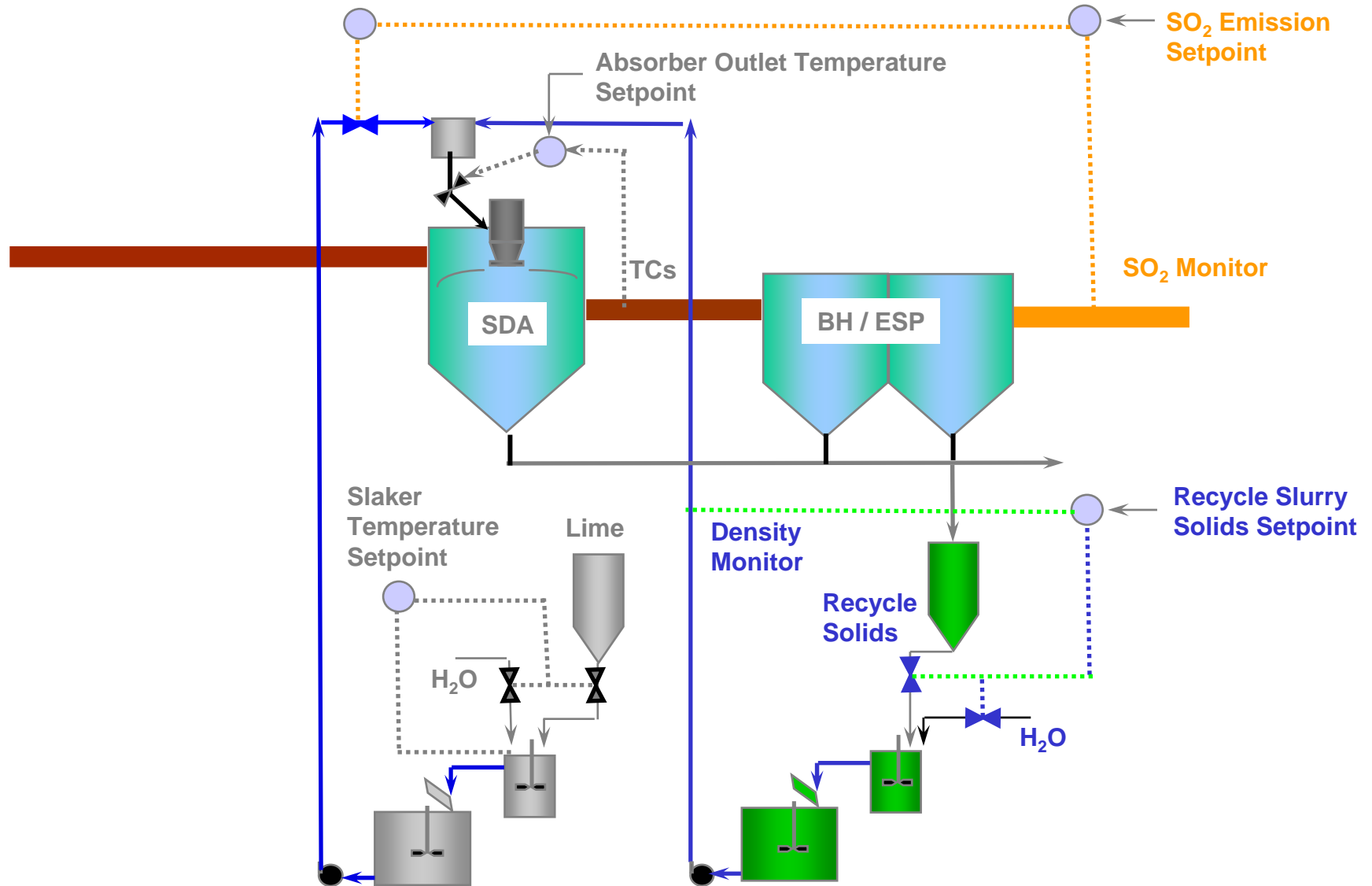
USA
Total generation 1,427,263 tons

SDA By-Product Solids Use (2004)

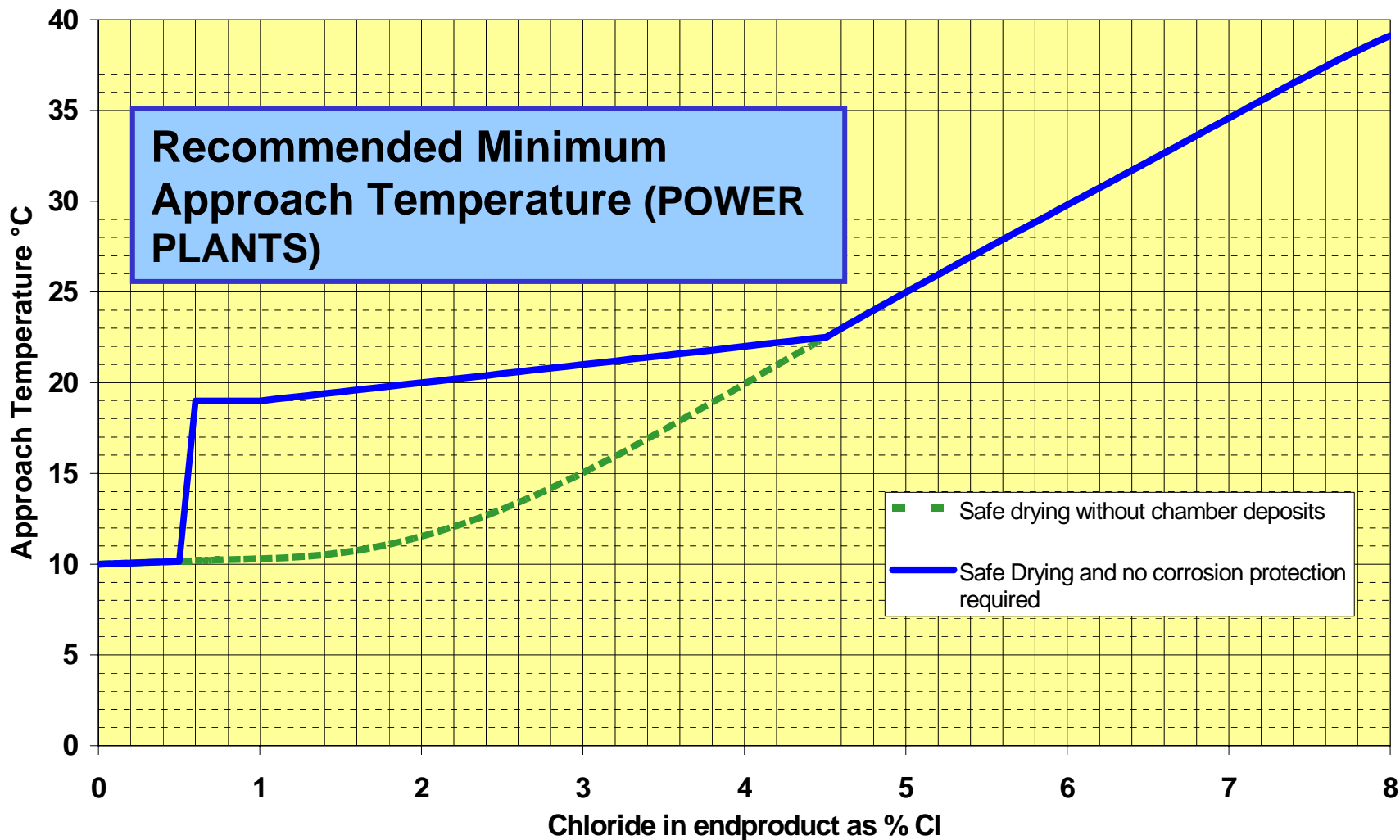








Recommended Operating Conditions
 (Feed solids >30% and limited amount of soluble salts)

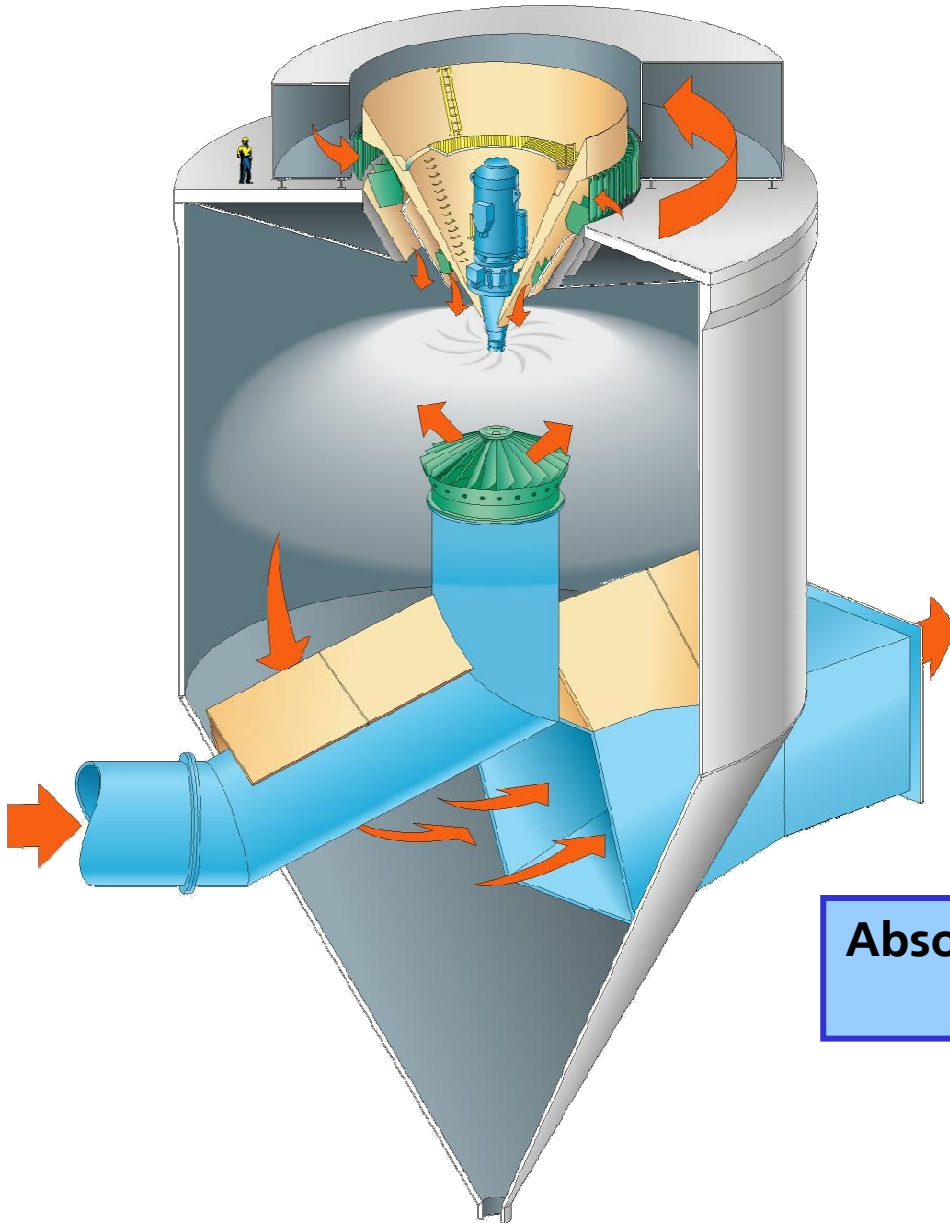




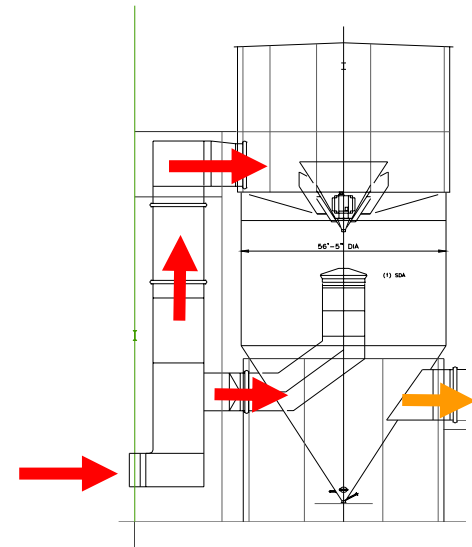


Add reagent
Dry slurry
Humidify gas

Collect solids
Continue reactions

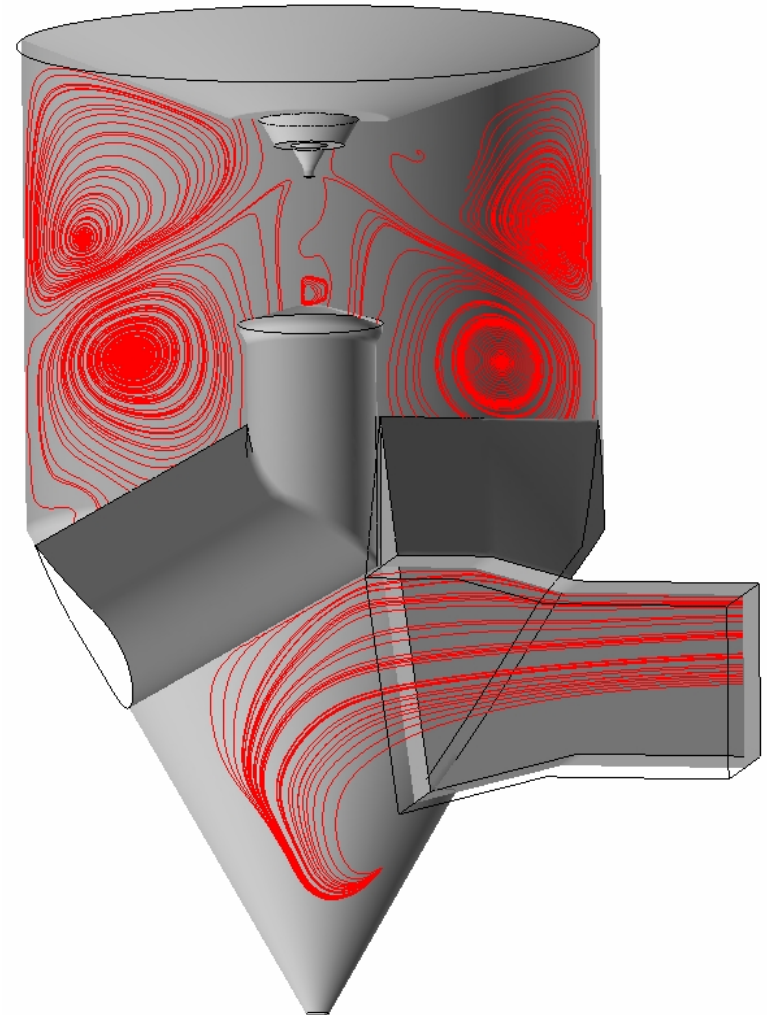
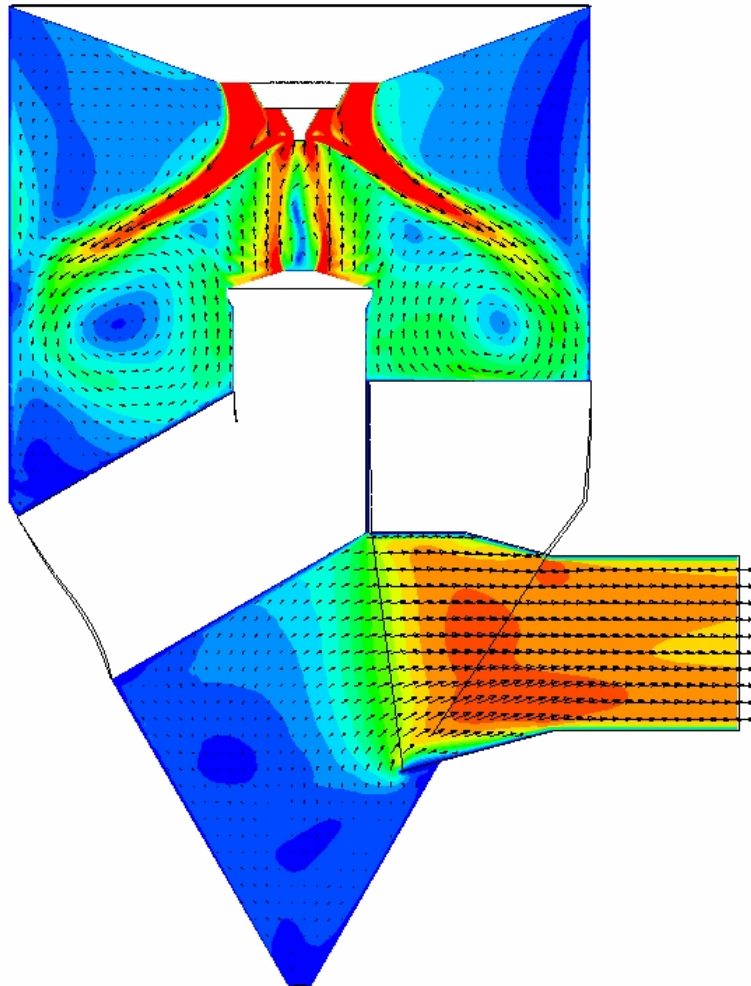


**Large modules
Typical for Power Plants**



Absorber diameter up to 20,3 m

CFD-modelling of Niro SDA size 20.000

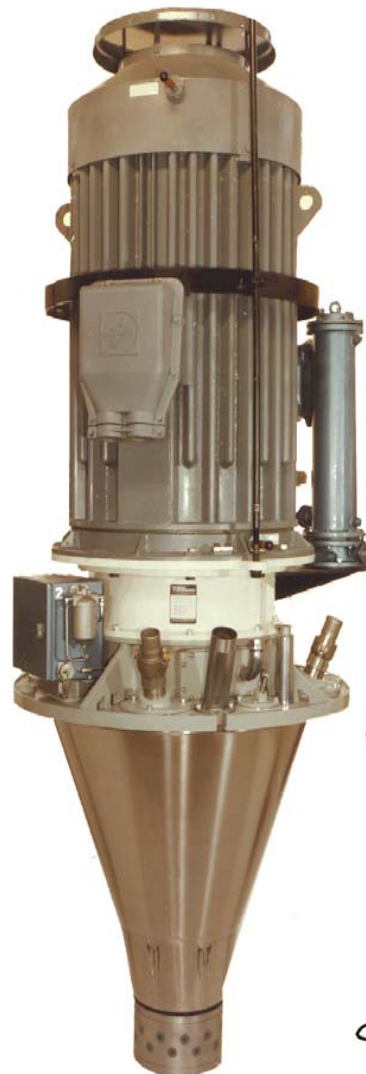


Atomizer Design



Rotary Atomizer Type F-100

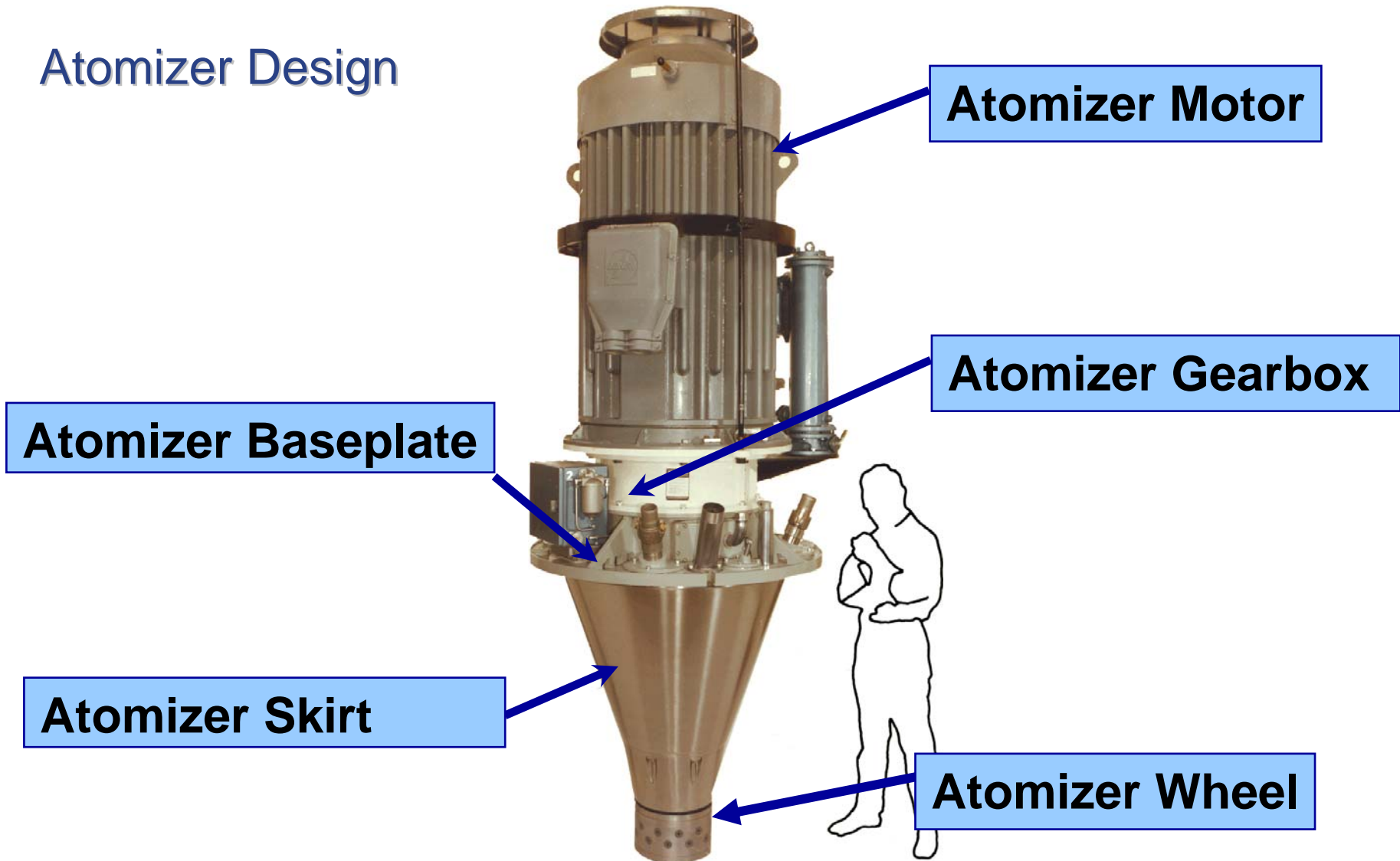
Motor max	75	kW
Max capacity	10	t/h
Wheel dia.	210	mm
Wheel rpm	13.500	
Periph. speed	148	m/s

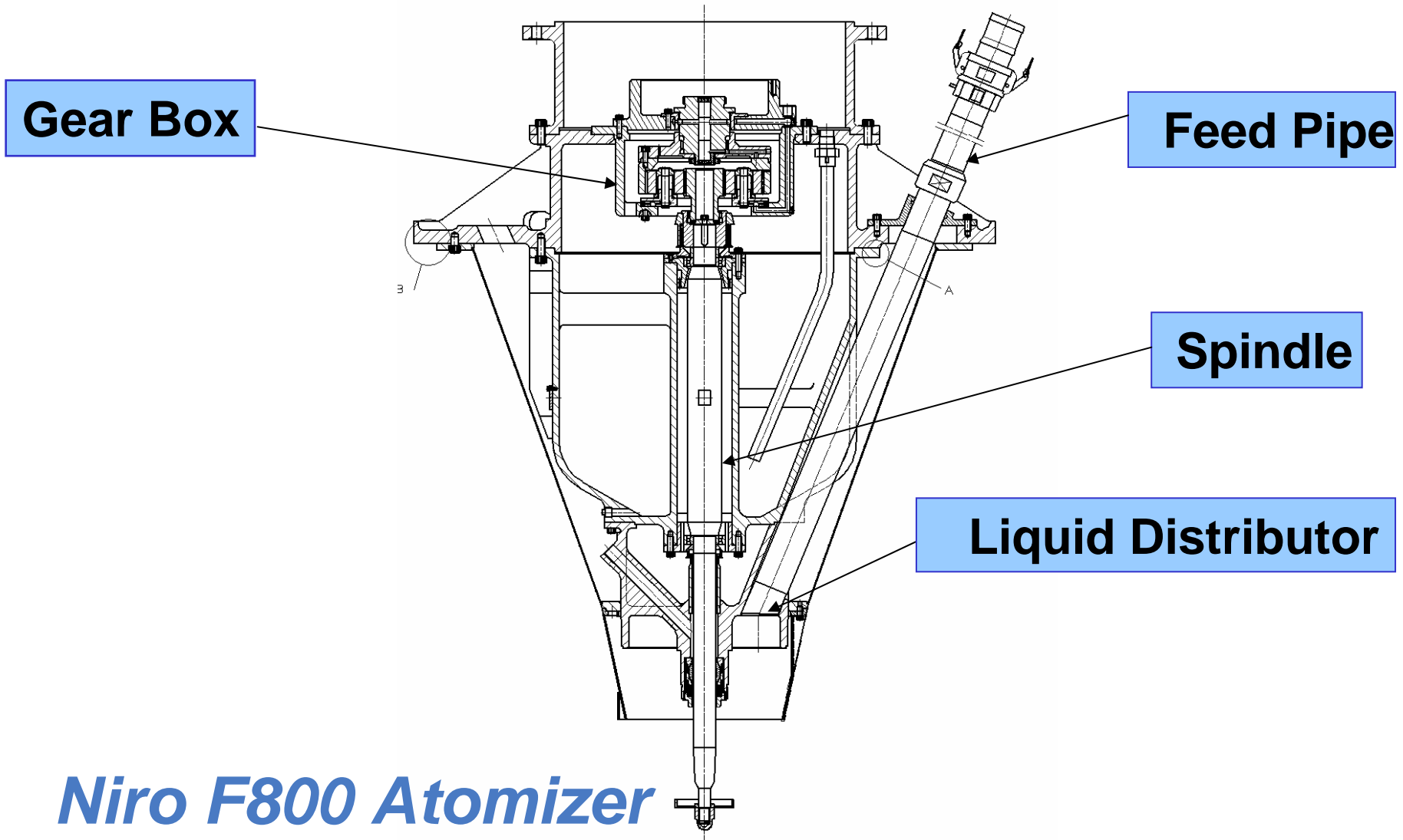


Rotary Atomizer Type F-800

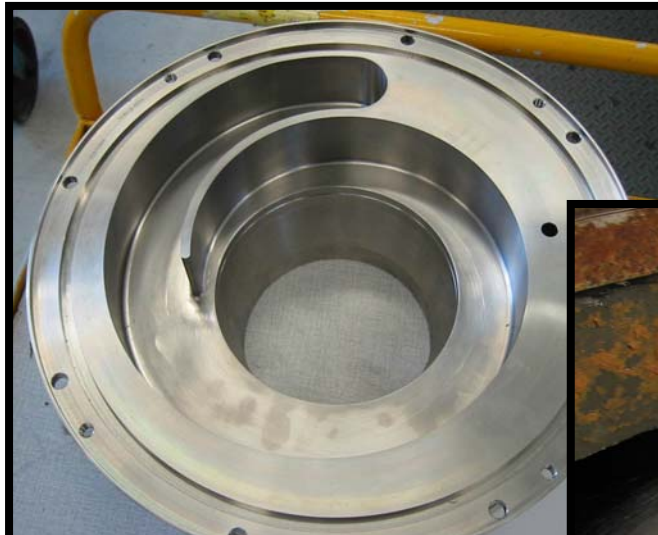
Motor max	800	kW
Max capacity	91	t/h
Wheel dia.	350	mm
Wheel rpm	9.550	
Periph. speed	175	m/s

Atomizer Design





Niro F800 Atomizer

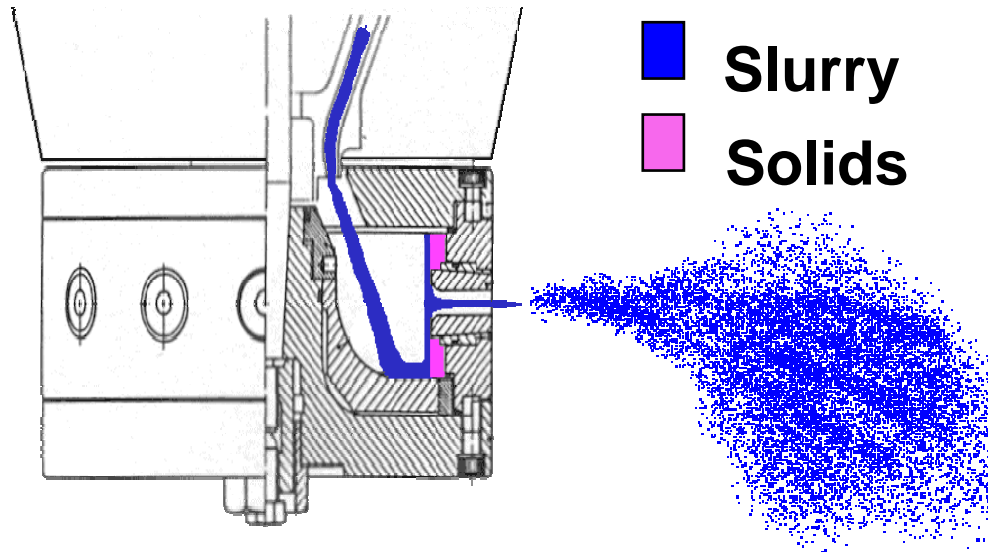


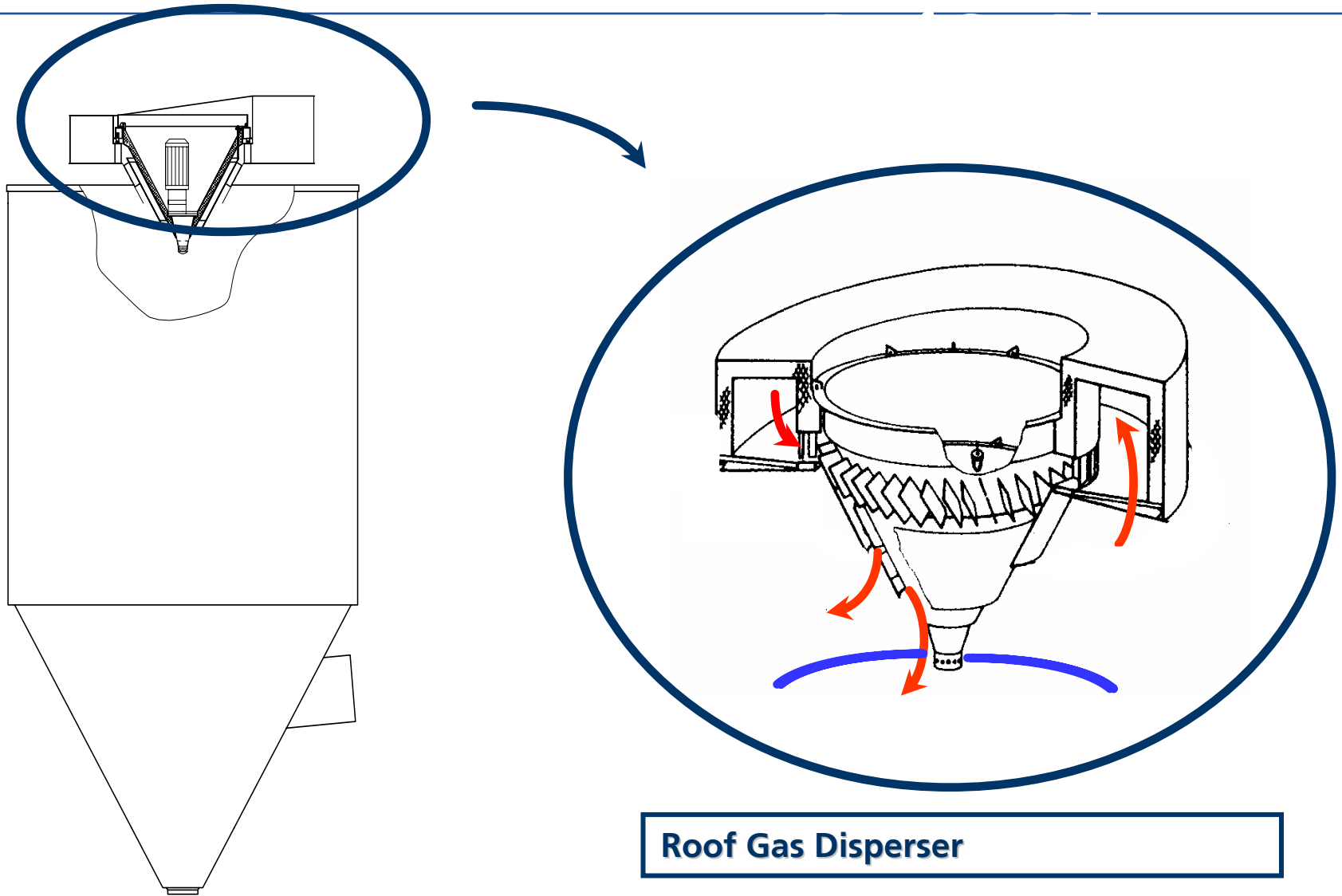
Niro Volute Liquid Distributor



Even slurry flow to wheel prevents imbalance

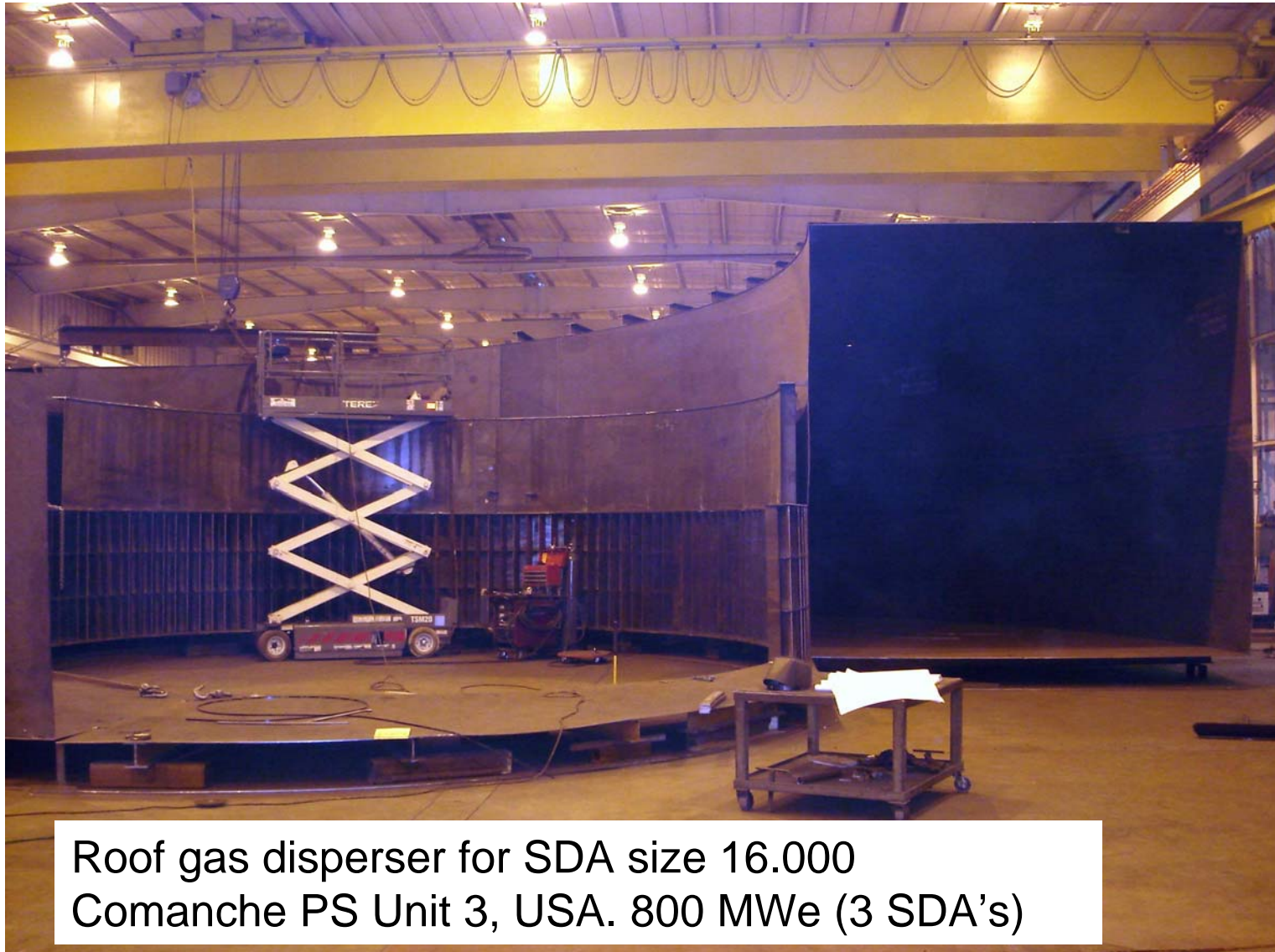
Atomizer Wheel







Roof Gas Disperser



Roof gas disperser for SDA size 16.000
Comanche PS Unit 3, USA. 800 MWe (3 SDA's)

Central Gas Dispenser





Lime Silo Bottom & Paste Slaker



Vertical Ball Mill

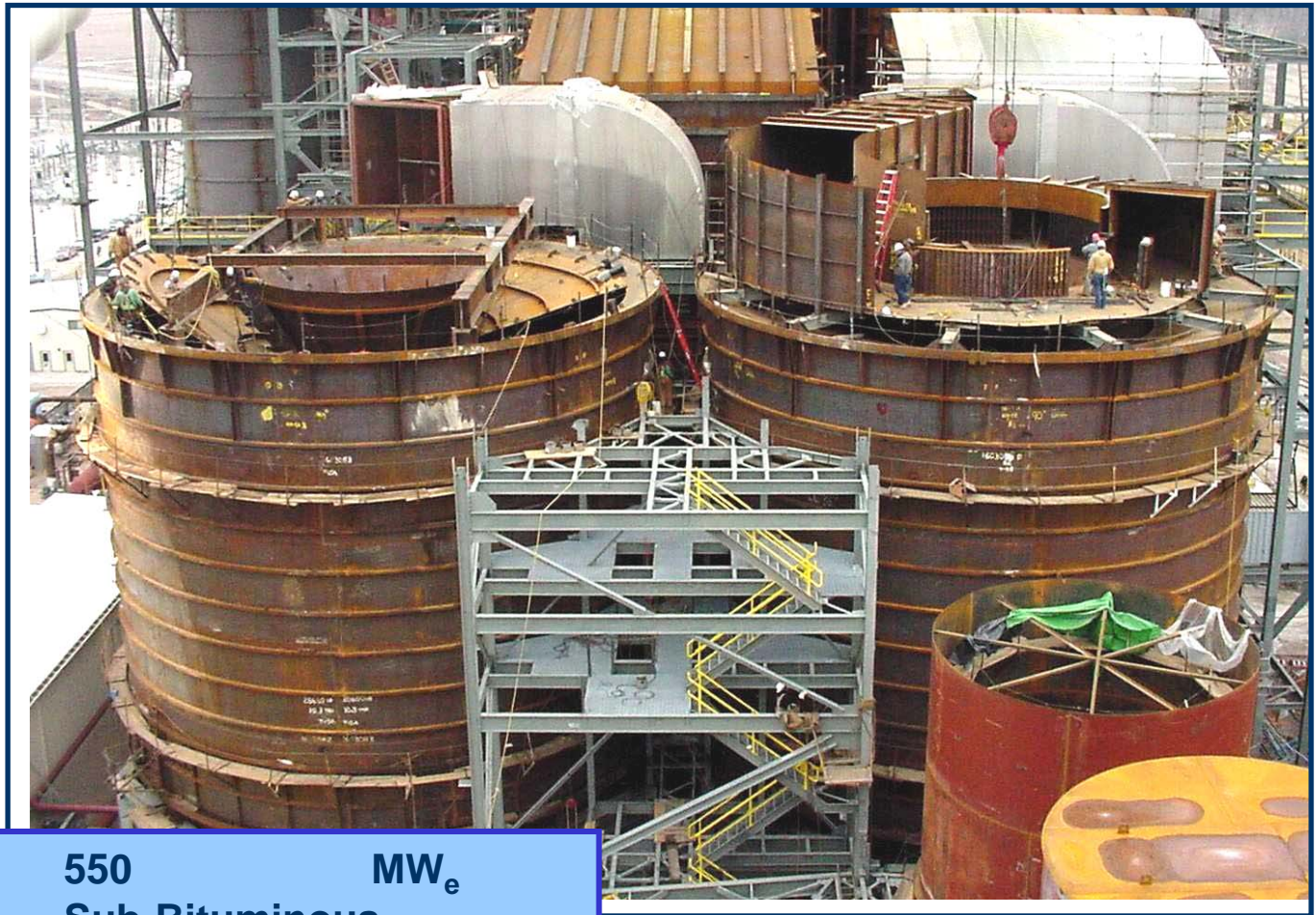


Detention Slaker



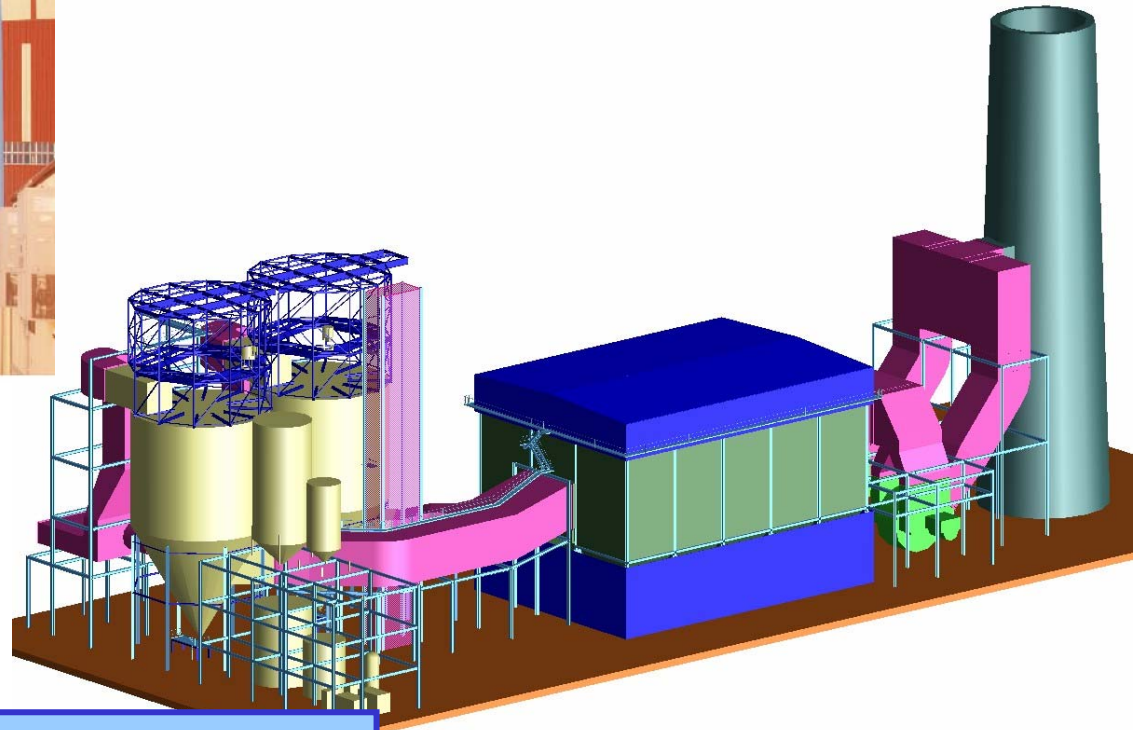
SDA Applications

**Hawthorn Power Station, Unit 5,
Kansas City,
Missouri, USA**



Boiler output	550	MW_e
Coal	Sub-Bituminous	
Sulfur content	0,2 - 0,7	%
Flue gas amount	1 x 2.150.000	Nm³/h
Chamber Diam.	17.2	m
Dust collector	Pulse-jet	

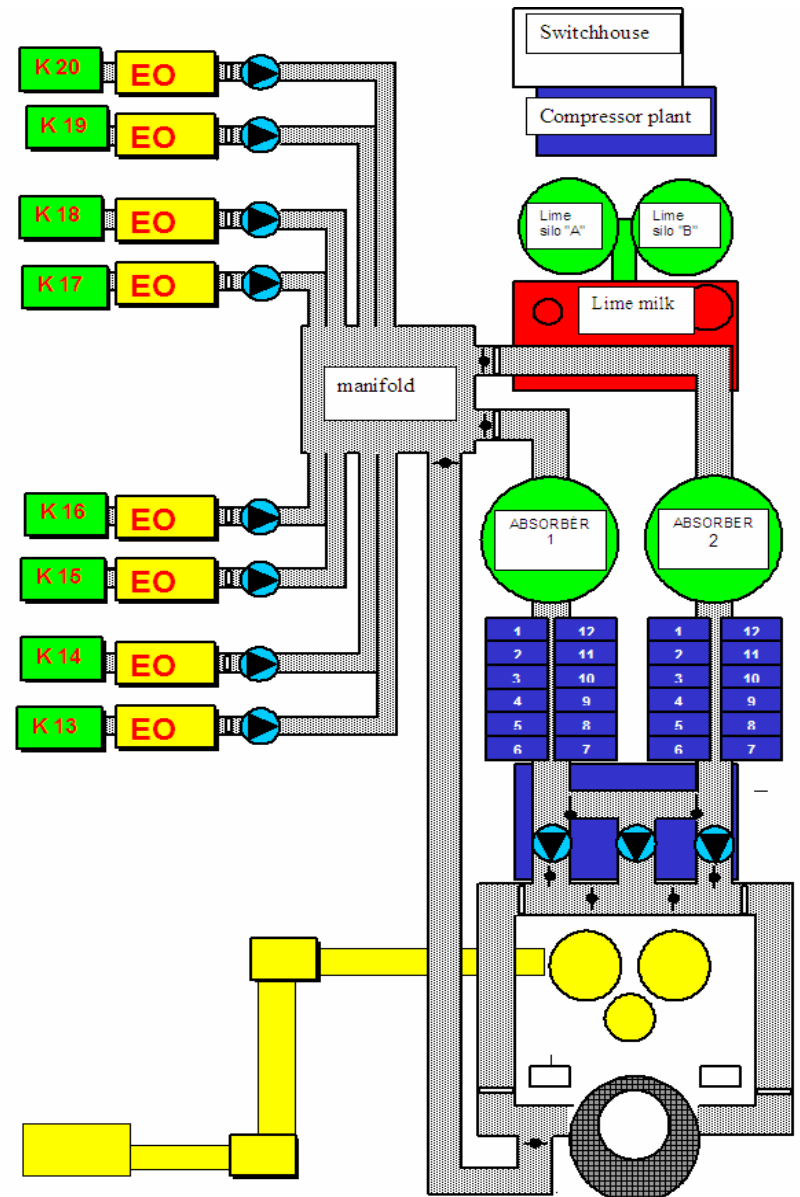
Weston 4 – Wisconsin Public Service



Boiler output	500	MW_e
Coal	Sub-Bituminous	
Sulfur content	0,2 - 0,6	%
Flue gas amount	1 x 2.150.000	Nm³/h
Chamber Diam.	17.2	m
Dust collector	Pulse-jet	

Layout,
Chemopetrol T700,
Czech Republic

440 MWe, total
8 parallel boilers
Precollection of fly ash
High turndown
requirement
2 SDA's
2 Fabric filters
2 Booster fans +1 spare



Kraftwerk Dürnrohr, Austria

Boiler output	390 + 335	MW _e
Coal	Mix	
Sulfur content	0,7-1	%
Fluegas amount	2 x1.100.000	Nm3/h
Chamber Diam.	13.2	m.
Dust collector	ESP	
Availability	>99	%



AVAILABILITY DATA

Installation			Year 1	Year 2
Studstrupvaerket MKS 3	Denmark	350 MWe	99.4	99.3
Studstrupvaerket MKS 4	Denmark	350 MWe	99.8	99.3
Duernrohr EVN	Austria	350 MWe	>99	100
Duernrohr VKG	Austria	410 MWe	>99	100
Salzburger Stadtwerke	Austria	112 MWt	99.3	>99
Mainkraftwerke	Germany	250 MWt	97.7	>97
Walheim	Germany	260 MWe	99.5	>99
Vaesteraas	Sweden	585 MWt	99.4	>99
Sherco, Unit 3	USA	900 MWe	100	>99
Rawhide, Unit 1	USA	275 MWe	100	>99
Holcomb Station, Unit 1	USA	280 MWe	98.7	98.2
Antelope Valley, Unit 1	USA	450 MWe	>99	>99
Antelope Valley, Unit 2	USA	450 MWe	>99	>99

Main features of spray drying absorption:

- High removal efficiency, SO₂, SO₃, HCl, HF etc.
- Low capital investment
- Entire flue gas path made of carbon steel
- No need for clean gas reheat
- Simple and robust system
- High availability
- Low water consumption
- Makes use of low quality process water
- No waste water production

